

Biological Design Automation for Optimal Cell Factories

Giuseppe Nicosia

Computational Synthetic & Systems Biology Lab

Dept. of Mathematics & Computer Science

University of Catania, Italy

www.dmi.unict.it/~nicosia/

BioCAD tools and algorithms

1. Optimisation
 1. Global/Local Optimisation
 2. Single/Multi-objective Optimisation (discrete for the genes and continuous for fluxes)
 3. ε -dominance Analysis
2. Sensitivity Analysis (SA)
 1. Reaction-oriented SA (RoSA)
 2. Species-oriented SA (SoSA)
 3. Pathway-oriented SA, discrete (Gene Sets) or continuous (Fluxes) (PoSA)
3. Robustness Analysis (RA)
 1. Global RA
 2. Local RA
 3. Glocal RA
 4. Pathway-oriented RA
4. Identifiability Analysis (Genotype-Phenotype relationships)

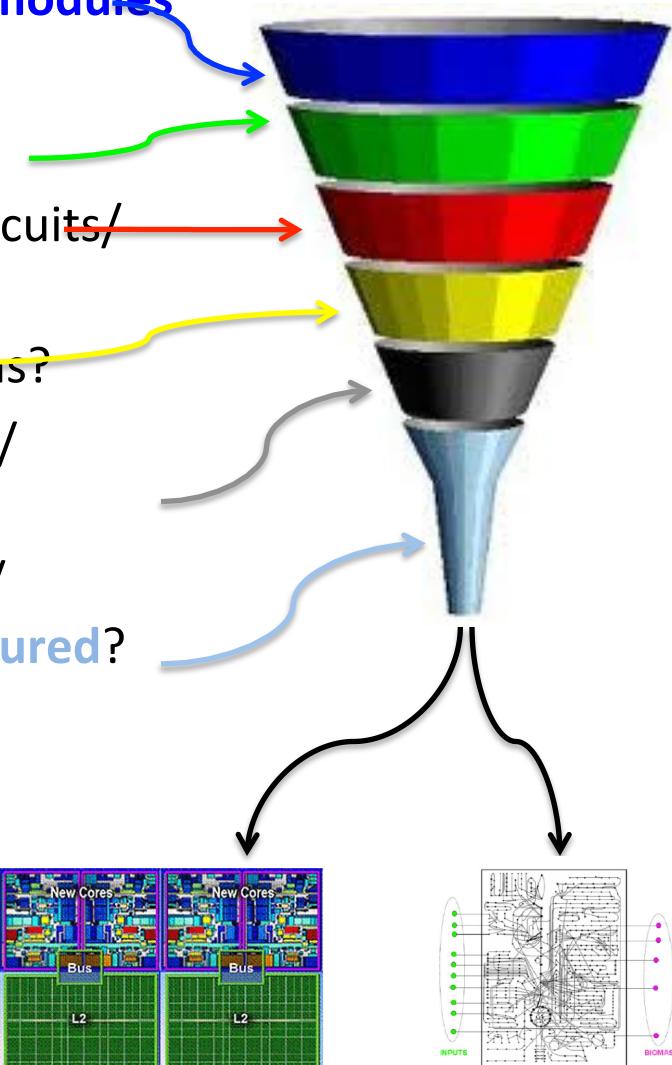
Requests in Electronic Design Automation

VS.

Biological Design Automation

$10^7\text{-}10^8$ candidate solutions/strains/pathways

- Which are **the most important parameters/parts/modules** of the given Device/Circuit/System* ?
- How many **Feasible** Devices/Circuits/Systems?
- How many **Optimal and/or Suboptimal** Devices/Circuits/Systems?
- How many **Pareto Optimal** Devices/Circuits/Systems?
- How many Robust Pareto Optimal Devices/Circuits/Systems?
- Which is the set of **Robust Pareto Optimal** Devices/Circuits/Systems that can be **successfully manufactured**?



* Device = gene/protein/enzyme
Circuit = pathway/organelle
Board/Chip = cell
System (system-of-systems) = tissue/organ/organism

Mixed Integer-Discrete-Continuous Constrained Multi-Objective Optimization Problem

Find

$$X = \{x_1, x_2, \dots, x_n\} = [X^{(i)}, X^{(d)}, X^{(c)}]^T$$

To Minimize/maximize

$$f_m(x), \quad m = 1, 2, \dots, M;$$

Subject to

$$g_j(x) \geq 0, \quad j = 1, 2, \dots, J;$$

$$h_k(x) = 0, \quad k = 1, 2, \dots, K;$$

$$x_i^{(L)} \leq x_i \leq x_i^{(U)} \quad i = 1, \dots, N.$$

Where $X^{(i)}$, $X^{(d)}$, $X^{(c)}$ denotes **feasible subsets of integer, discrete and continuous variables respectively**. While both integer and discrete variables have a discrete nature, only discrete variables can assume floating point values (*they are often unevenly spaced*): $[L_i, U_i, S_i]$
Integer and discrete variables required different handling.

If a solution x satisfies all of the **(J+K) constraints** and all of the **2N variable bounds**, it is known as a **feasible solution**.

Design variables: fluxes and/or gene sets, or Down- and Up- Regulation of Enzymes

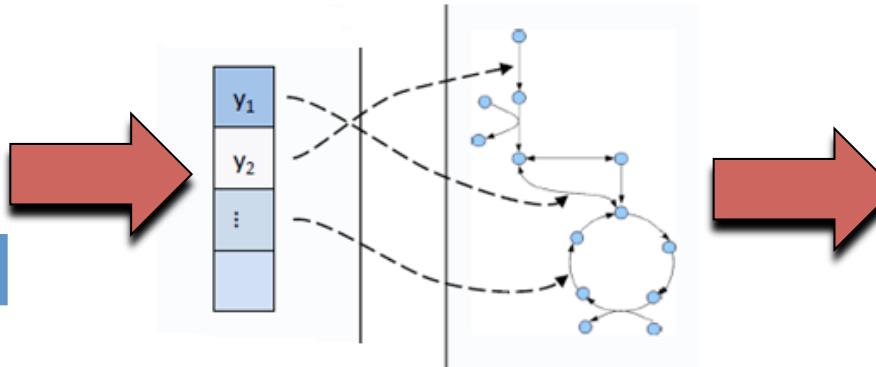
Objective functions: Biomass vs. ATP, Biomass vs. Succinate (Ethanol, 1,4Butanediol)

Constrains: $O_2=0$, $GLC \geq 10$, $5 \leq Ca \leq 10$, Ph value

Genetic Design via MOO

$y_{34} = 1$
 $y_{784} = 1$
 $y_{432} = 1$

0	1	0	1	0	0	...	0
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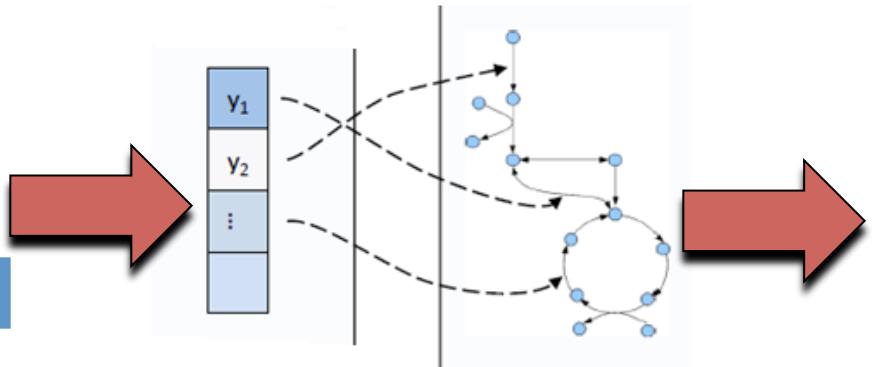


Acetate = + 66%
with respect to
Wild Type

Knockout = 3

$y_{63} = 1$
 $y_{222} = 1$
 $y_{562} = 1$
 $y_{24} = 1$

0	1	0	1	0	1	...	1
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Acetate = + 130%
with respect to
Wild Type

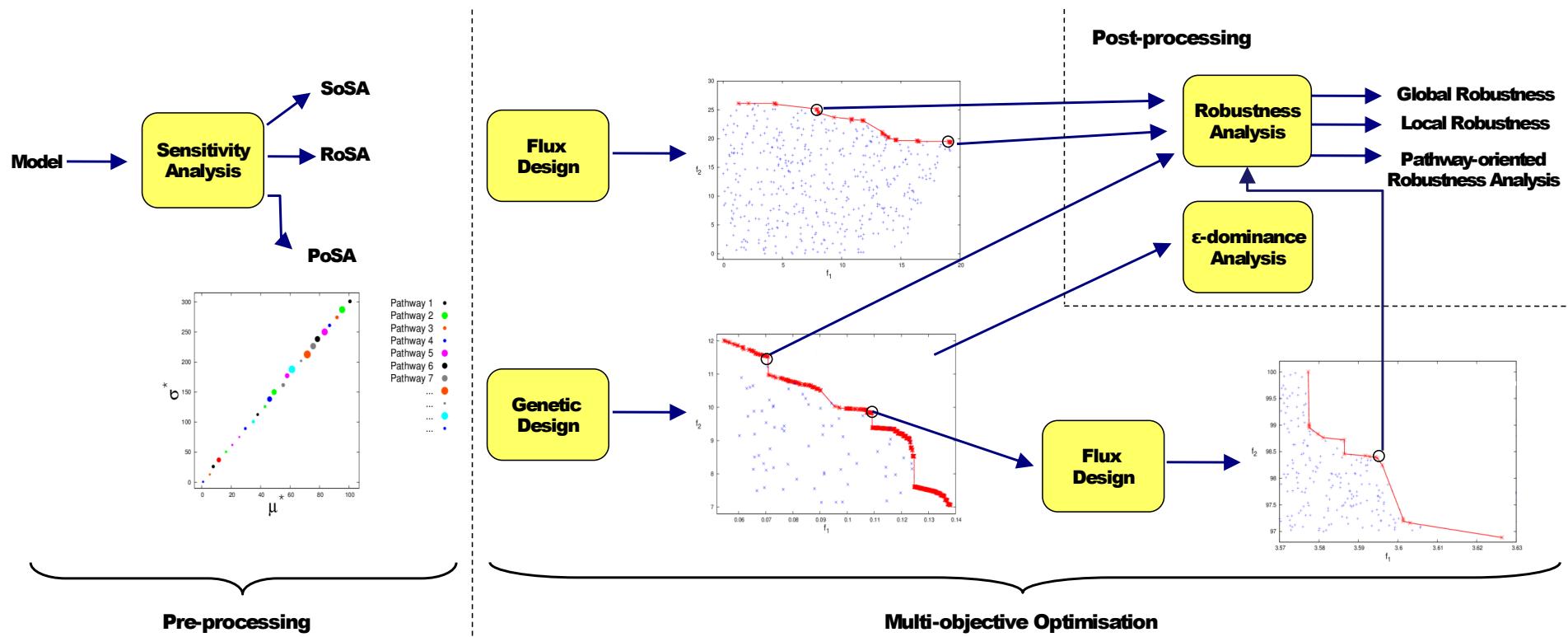
Knockout = 4

optBioCAD

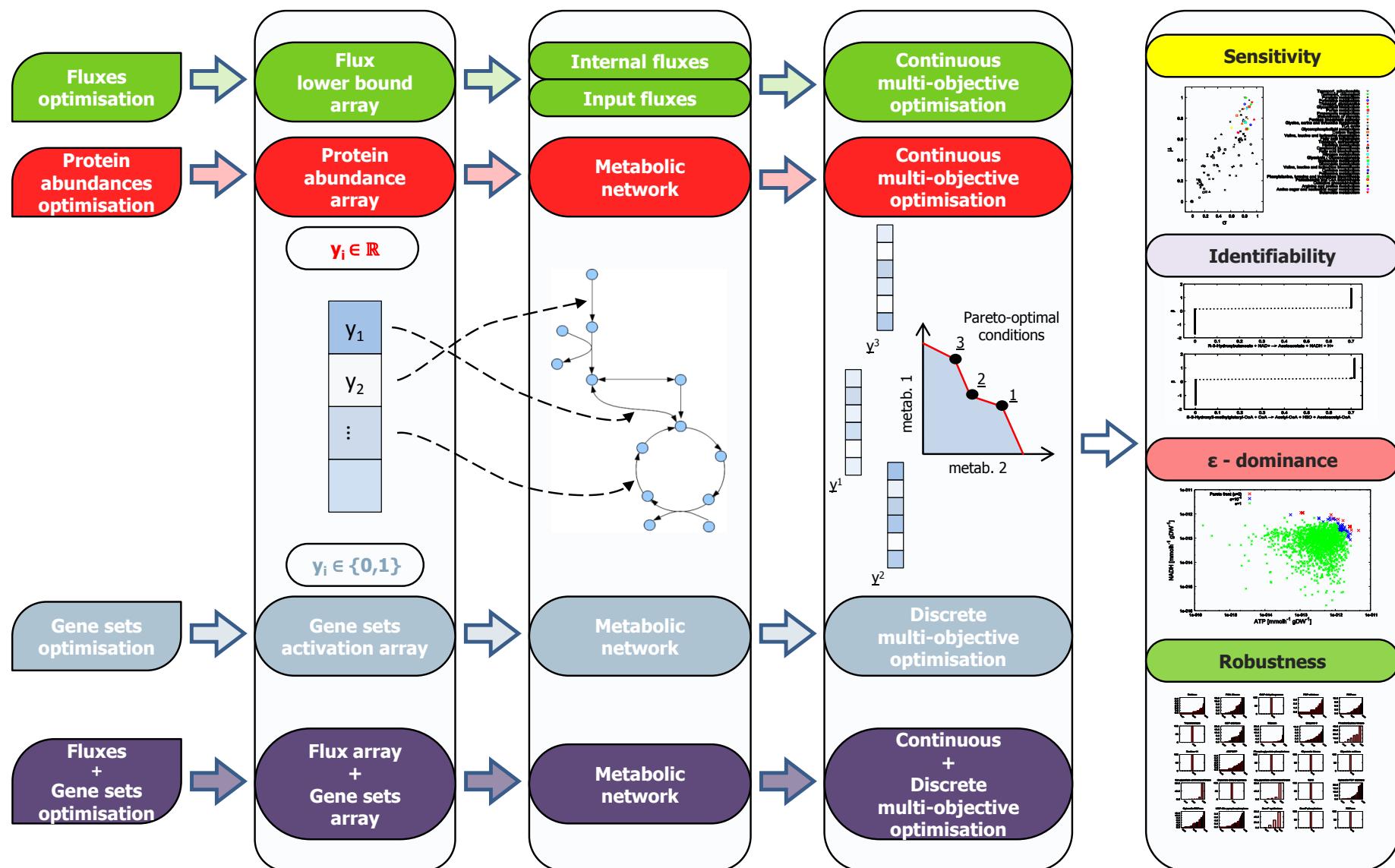
Algorithm 1 OPTBIOCAD Pseudo-code.

```
1: optBioCAD (model, d, dup,  $\tau_B$ ,  $\rho$ ,  $\beta$ ,  $s_a$ )
2:  $t \leftarrow 0$ ;
3:  $BC_{arch} \leftarrow Create\_Archive(s_a)$ ;
4:  $P^{(t)} \leftarrow Initialise(d)$ ;
5: Evaluate( $P^{(t)}$ , model);
6: EvaluateConstraints( $P^{(t)}$ , model);
7: while  $\neg Stop\_Condition(t)$  do
8:    $P_{cop} \leftarrow Copying(P^{(t)}, dup)$ ;
9:    $P_{LS} \leftarrow Local\_Search\_Operator(P_{cop}, \rho)$ ;
10:   $P_{GS} \leftarrow Global\_Search\_Operator(P_{hyp}, \beta)$ ;
11:  Evaluate( $P_{GS}$ , model);
12:  EvaluateConstraints( $P_{GS}$ , model);
13:  Diversity_Enforcing( $P^{(t)}$ ,  $P_{GS}$ ,  $\tau_B$ );
14:   $BC_{arch} \leftarrow (BC_{arch} \cup P^{(t)} \cup P_{GS})$ ;
15:   $P^{(t+1)} \leftarrow Selection(P^{(t)}, P_{GS}, BC_{arch})$ ;
16:   $t \leftarrow t + 1$ ;
17: end while
18: return ( $P^{(t)}$ ); /* output the best d candidate solutions */
```

Design Flow – 1/2



The Overall Design Flow – part 2/2



E. coli Designing

Designing Molecular Machines

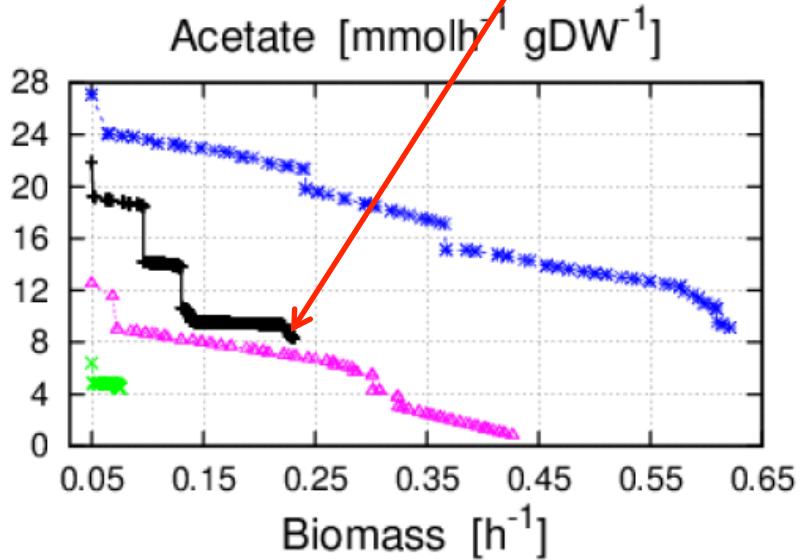
We test the computational framework in the genome-scale metabolic network of *E. coli* iAF1260 (Feist et al., 2007)

- 2382 reactions (299 exchange fluxes)
- 1039 metabolites
- 913 gene sets (1040 in E. coli 2011)
- 1260 genes
- 36 pathways
- 3 compartments

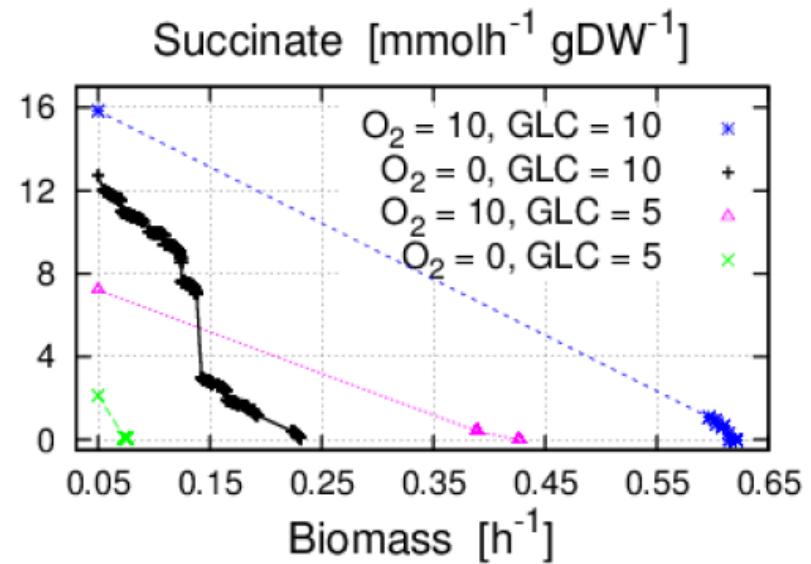
Aim: maximise a metabolite of interest (e.g., acetate/succinate), and simultaneously ensure the *biomass formation*, with the *minimum knockout cost*.

Acetate vs. Biomass & Succinate vs. Biomass Pareto Fronts

A



B



- A) Acetate vs. Biomass maximisation in ***different environmental conditions***
B) Succinate vs. Biomass maximisation in ***different environmental conditions***

Supplementary Table 1 - Microsoft Excel

Home Inserisci Layout di pagina Formule Dati Revisione Visualizza

Times New Rom 11 A A Testo a capo Generale Numeri Allineamento Unisci e centra Formattazione condizionale Formatta come tabella Stili cella Inserisci Elimina Formato Celle Somma automatica Riempimento Cancella Ordina e filtra e seleziona Modifica

G1 ffx

A B C D E F

1 Pareto Front obtained by the 2-objective optimisation to maximise the acetate production and biomass formation in E.coli (parameters of GDMO: pop=1000, gen=1500)

2 Anaerobic condition, GLC = 10 mmolh-1 gdW-1, values in brackets represent the variation with respect to the wild type configuration

3

4 Acetate Biomass Knockout Genes Pathways Reactions

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6 8,3014 0,23106 0

7

8 14,1962 0,096328

9 (71.0095%) (-58.2994%)

10 11 (((b0351)_OR_(b1241))))
(((b0870)_OR_(b2551))))

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21 13,7911 0,13035

22 (66.13%) (-43.5725%)

23 3 (((b0351)_OR_(b1241))))
((b1539))

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27 18,4549 0,096233

28 (122.3111%) (-58.3406%)

29 11 (((b0351)_OR_(b1241))))
(((b2975)_OR_(b3603))))

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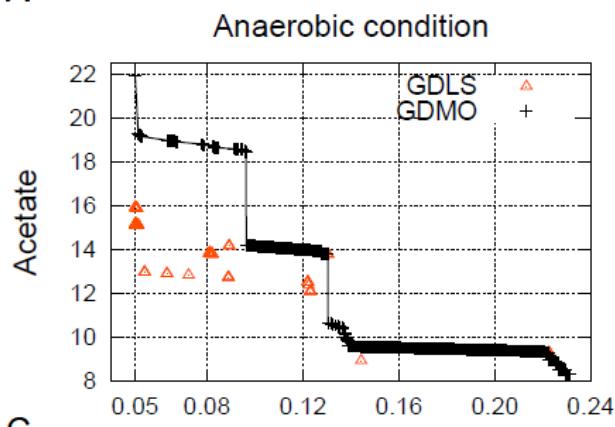
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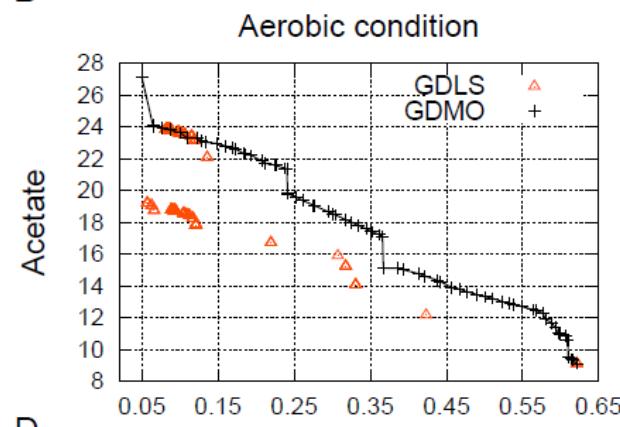
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GDMO (us) vs. GDLS (G. Church)

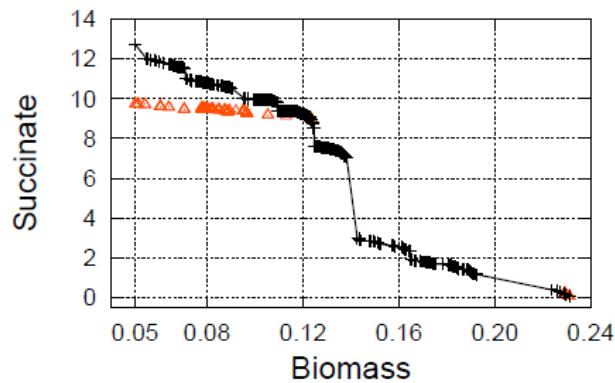
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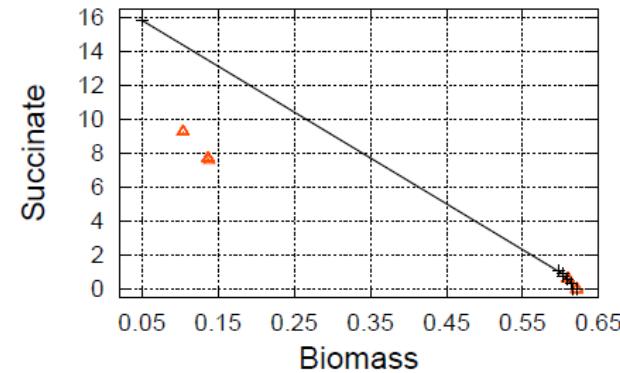
B



C



D



Black: Pareto front obtained by GDMO.

Red: optimal results obtained by GDLS [G. Church, Lun et al., Molecular Systems Biology, 2009]
[G. Church et al, PLOS Comp. Biol. 2013]

OptFlux (*Rocha et al, BMC Bioinf '08*)

OptGene (*Patil et al, BMC Bioinf '05*)

GDLS (*Lun, G. Church et al, MSB '09*)

OptKnock (*Bugard et al, Biotech & Bioeng'03*)

GDBB (*Lun et al, Bioinformatics'12*)

GDMO vs. OptGene, OptFlux,
OptKnock, GDLS, GDBB

	Wild Type	OptFlux [1]	OptGene [2]	GDLS [3]	GDLS [3]	OptKnock [4]	OptKnock [4]	GDMO	GDMO	GDMO
Acetate	8.30	15.129	15.138	15.914	n.a.	n.a.	12.565	13.797	19.150	n.a.
Succinate	0.077	10.007	9.874	n.a.	9.727	9.069	n.a.	n.a.	n.a.	10.610
Biomass [1/h]	0.23	n.a.	n.a.	0.0500	0.0500	0.1181	0.1165	0.1296	0.053	0.087
K cost	n.a.	n.a.	n.a.	14	26	54	53	3	10	8

[1] Rocha M et al. (2008) Natural computation metaheuristics for the in silico optimization of microbial strains. MC Bioinformatics 9: 499

[2] Patil K et al. (2005) Evolutionary programming as a platform for in silico metabolic engineering. BMC Bioinformatics 6: 308

[3] Lun DS et al. (2009) Large-scale identification of genetic design strategies using local search. Molecular Systems Biology 5

[4] Bugard Apat al. (2003) Optknock: a bilevel programming framework for identifying gene knockout strategies for microbial strain optimization. Biotechnology and Bioengineering 84: 647657

Robustness Analysis - E. coli iAF1260

- GR: Global Robustness [1]
- LR: Local Robustness [1]
- R: Glocal Robustness [2]
- PoRA: Pathway-oriented Robustness [3]

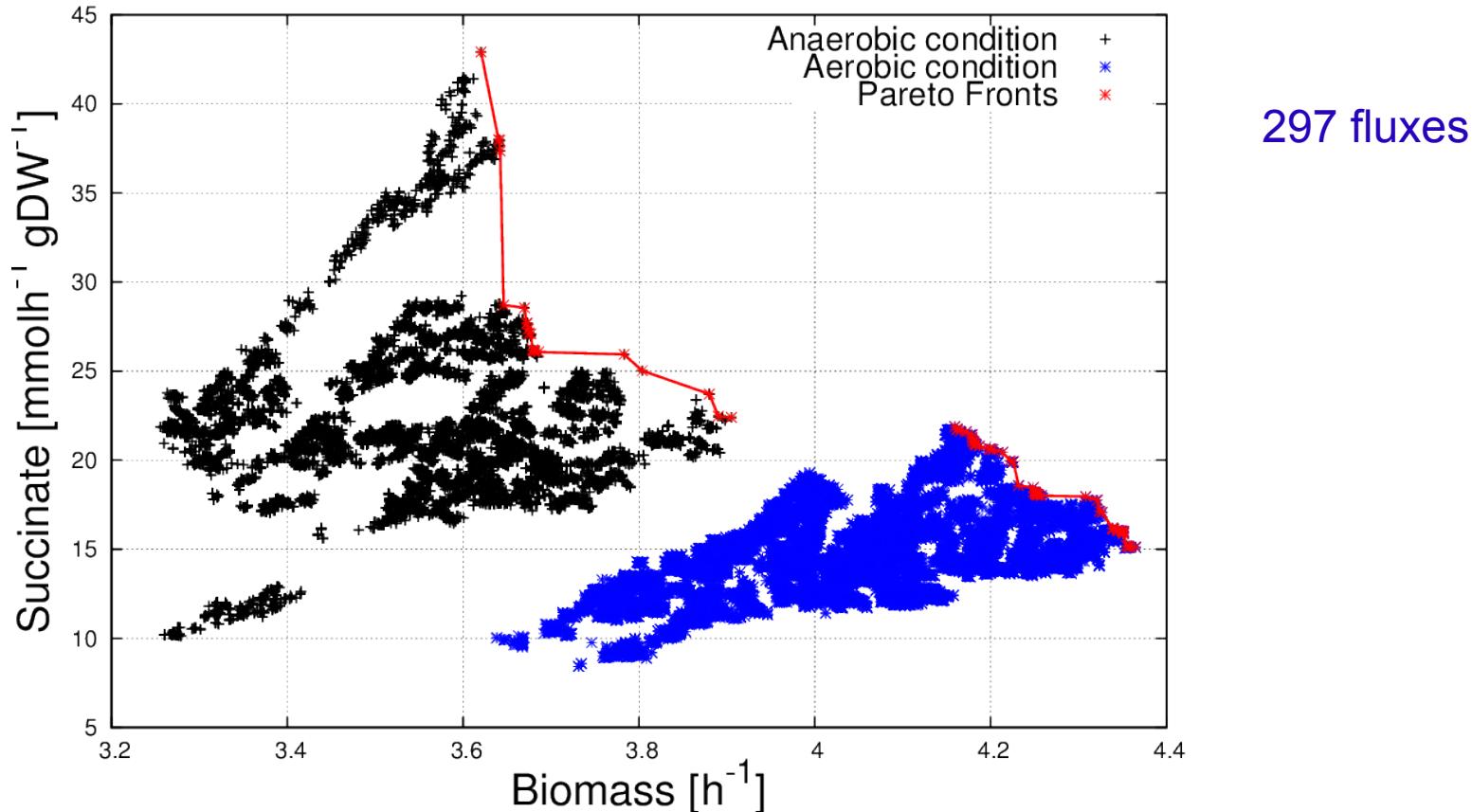
- [1] Stracquadanio, G., and Nicosia, G. (2011) Computational energy-based redesign of robust proteins. *Comput. Chem. Eng.*
- [2] Hafner, M. et al. (2009) ‘Glocal’ robustness analysis and model discrimination for circadian oscillators. *PLoS Comput. Biol.*
- [3] Nicosia et al. (2012) Robust Design of Microbial Strains. *Bioinformatics J.*

	Wild Type	OptFlux	OptGene	GDLS	GDLS	OptKnock	OptKnock	GDMO	GDMO	GDMO
Acetate	8.30	15.129	15.138	15.914	n.a.	n.a.	12.565	13.797	19.150	<i>n.a.</i>
Succinate	0.077	10.007	9.874	n.a.	9.727	9.069	n.a.	<i>n.a.</i>	<i>n.a.</i>	10.610
Biomass [1/h]	0.23	n.a.	n.a.	0.0500	0.0500	0.1181	0.1165	0.1296	0.053	0.087
K cost	n.a.	n.a.	n.a.	14	26	54	53	3	10	8
GR (%)	54.76/53.68	n.a.	n.a.	13.76	16.6	43.24	43.08	45.32	27.6	40.40
LR(%)	54.0/54.67	n.a.	n.a.	16.0	21.33	40.0	40.60	39.33	24.0	46.0
R	1.30/1.34	n.a.	n.a.	1.45	1.45	1.18	1.02	0.78	0.44	1.32
PoRA(%)	100.0/99.33	n.a.	n.a.	19.33	28.67	87.33	76.67	81.33	43.33	83.33

The Robustness estimates how robust is a strain when it undergoes small perturbations

Flux Design in *E. coli* iAF1260

Power law & specific operational regions

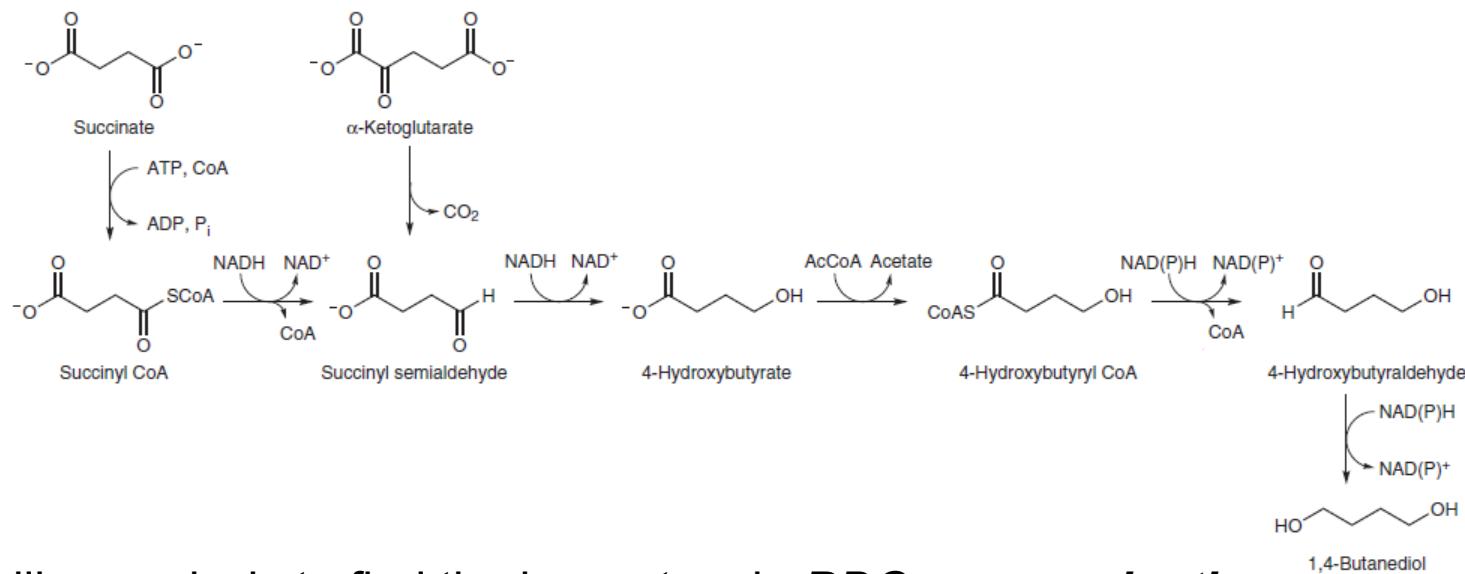


Overproduction of BDO in *E. coli* **optBioCAD/GDMO vs. Genomatica Inc. (and BASF)**

- 2 Genome-scale metabolic networks of *E. coli* (iJR904 and iJO1366)
(Palsson et al. *Gen. Biol.* 2003, *Mol. Syst. Biol.* 2011)
 - 931/2251 reactions
 - 625/1136 metabolites
 - 904/1366 genes
 - 729/1041 enzymes
- Synthetic pathway of **1,4 butanediol** (BDO)
- Genetic and Flux Design to overproduce BDO in *E. coli*
- BioCAD software

1,4-Butanediol

- BDO is an inorganic compound; it is used industrially as a solvent and in the manufacture of some types of plastics, elastic fibers and polyurethanes
- BDO currently is manufactured entirely from petroleum-based feedstocks
- Inclusion of BDO synthetic pathway in *E. coli* model – **BDO production**



- In silico analysis to find the key actors in **BDO overproduction**

BioCAD results

Deletions			Max BIO_ECO	EX_14btd(e) at Max BIO_ECO
ADHEr	LDH_D		0,378	5,72
ADHEr	LDH_D	MDH	0,296	7,72
ADHEr	LDH_D	CO2t	0,363	6,88
ADHEr	LDH_D	PTAr	0,219	6,60
ADHEr	LDH_D	ACKr	0,219	6,60
ADHEr	LDH_D	THD2	0,367	6,56
ADHEr	LDH_D	PGI	0,195	6,21
ADHEr	LDH_D	TPI	0,199	6,13
ADHEr	LDH_D	FUM	0,250	6,04
ADHEr	LDH_D	C140SN	0,307	5,94
ADHEr	LDH_D	TKT2	0,375	5,86
ADHEr	LDH_D	GLCpts	0,333	5,83
ADHEr	LDH_D	GLUDy	0,352	5,78
ADHEr	LDH_D	RPE	0,376	5,78
ADHEr	LDH_D	PFK	0,360	5,76
ADHEr	LDH_D	FBA	0,360	5,76
ADHEr	LDH_D	FRD3	0,368	5,74
ADHEr	LDH_D	NADH8	0,368	5,74
ADHEr	LDH_D	CBMK2	0,374	5,73
ADHEr	LDH_D	MDH FORt	0,140	15,17
ADHEr	LDH_D	PFLi MDH	0,140	15,17
ADHEr	LDH_D	MDH ATPS4r	0,203	12,17
ADHEr	LDH_D	PGDHY PGI	0,131	11,86
ADHEr	LDH_D	EDA PGI	0,131	11,86
ADHEr	LDH_D	FUM ACKr	0,127	10,92

203 solutions/strains

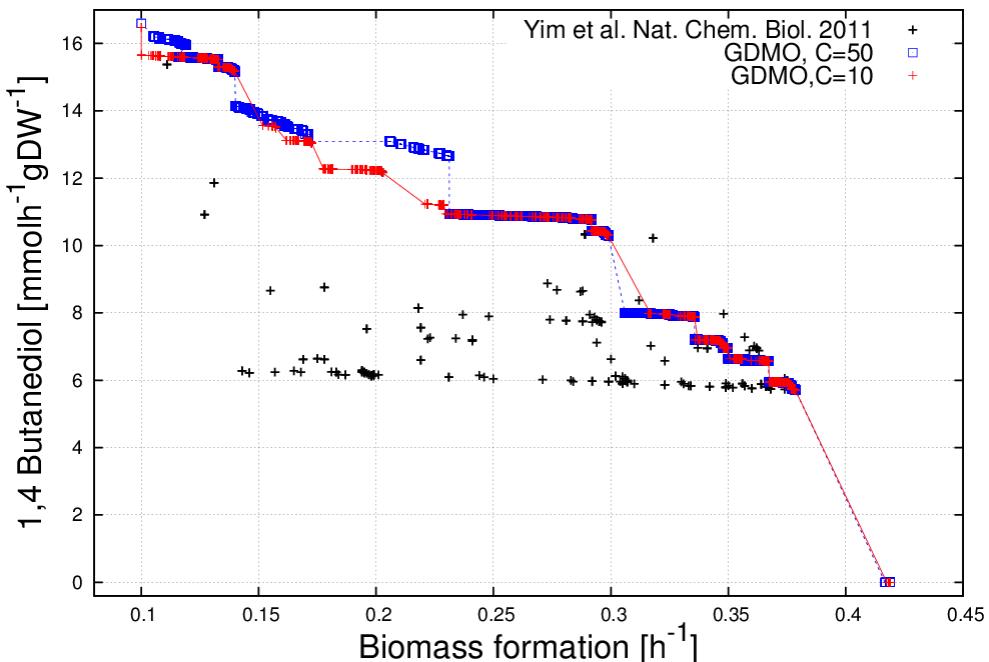
ADHEr	[c] : accoa + (2) h + (2) nadh <==> coa + etoh + (2) nad	
LDH_D	[c] : lac-D + nad <==> h + nadh + pyr	
MDH	[c] : mal-L + nad <==> h + nadh + oaa	
PFLi	[c] : coa + pyr --> accoa + for	
ADHEr	b1241	1
LDH_D	b2133 OR b1380	2
MDH	b3236	1
PFLi	(b0902 AND b0903 AND b2579) OR (b3114) OR (b3951 AND b3952)	3

Knockout cost = 7

From Yim H. et al. Metabolic engineering of Escherichia coli for direct production of 1,4-butanediol. Nat Chem Biol. 2011

BioCAD results

- MOO to maximise BDO production and biomass formation in synthetic *E.coli* model *iJR904*^[1]



Pareto fronts obtained by **GDMO** algorithm^[2]

- C=10 (12836 Pareto strains)
- C=50 (49876 Pareto strains)

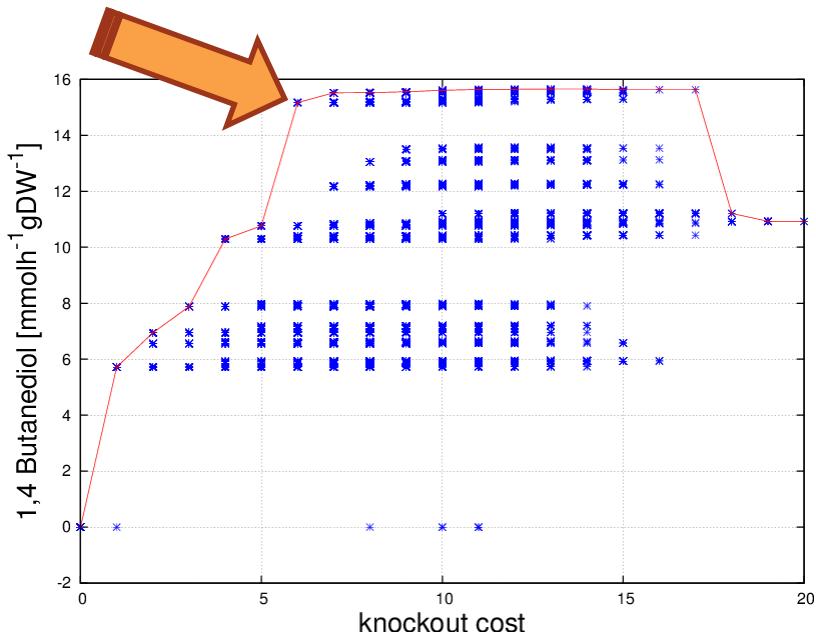
versus 203 solutions

C is the maximum knockout number allowable

[1] Reed et al. An expanded genome-scale model of *Escherichia coli* K-12 (*iJR904* GSM/GPR) Gen. Biol. 2003

[2] Nicosia et al. (2012) Robust Design of Microbial Strains. Bioinformatics

BioCAD results



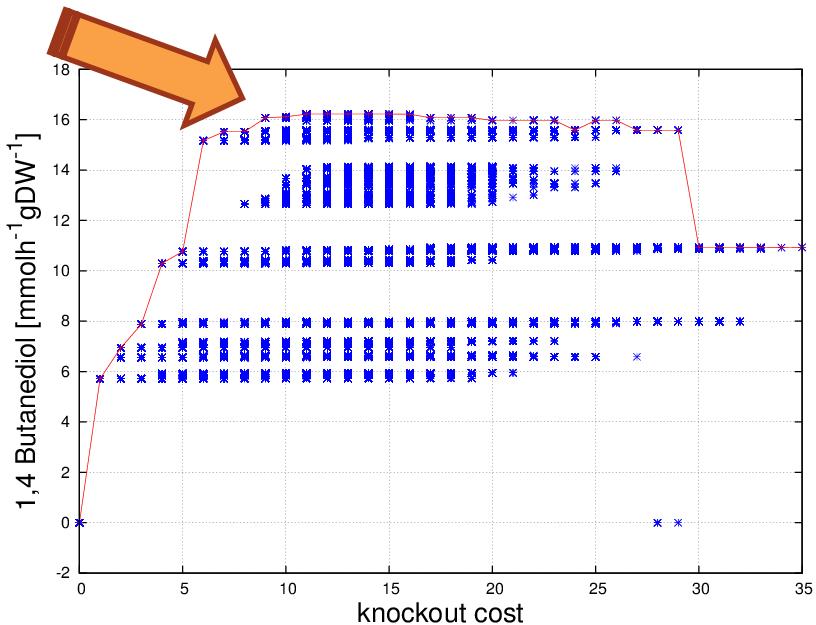
12836 Pareto optimal strains (C=10)

vs BDO=15,1660 & Biomass=0,1398

ADHER	b1241
LDH_D	b2133 OR b1380
MDH	b3236
PFLi	(b0902 AND b0903 AND b2579) OR (b3114) OR (b3951 AND b3952)

BDO	Biomass	kcost	Gene knockout	Pathway	Reactions
15.1683	0.13977 (-66.6334%)	6	b1241	Alternate Carbon Metabolism, Pyruvate Metabolism	LCADI , ADHER
			b3236	Citrate Cycle (TCA)	MDH
			b2975, b3603	Transport (Extracellular)	D-LACt2, GLYCLTt2r L-LACt2
			b2492, b0904	Transport (Extracellular)	FORt

BioCAD results



49876 Pareto optimal strains (C=50)

vs BDO=15,1660 & Biomass=0,1398

ADHER	b1241
LDH_D	b2133 OR b1380
MDH	b3236
	(b0902 AND b0903 AND b2579) OR (b3114) OR
PFLi	(b3951 AND b3952)

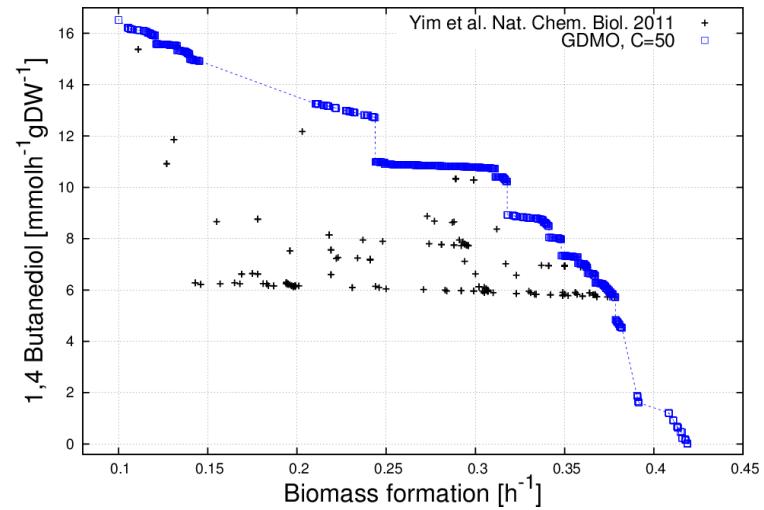
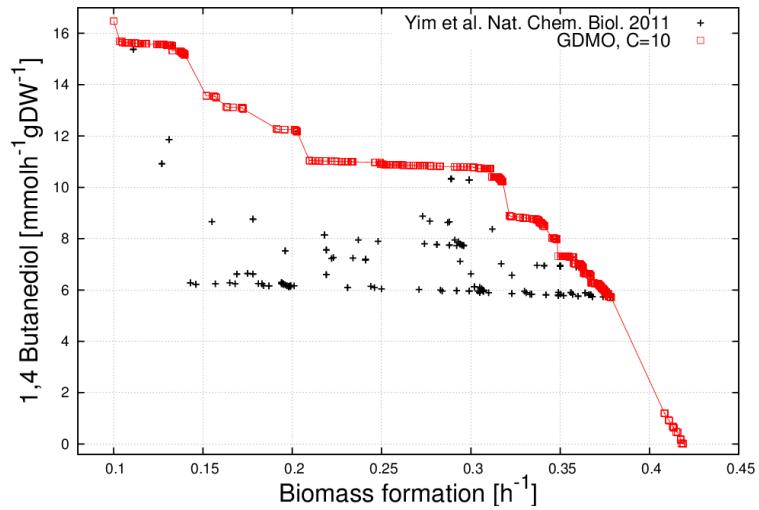
BDO	Biomass	kcost	Gene knockout	Pathway	Reactions
16.0736	0.11551 (-72.4245%)	9	b1241	Alternate Carbon Metabolism , Pyruvate Metabolism	LCADI, ADHER
			b2661	Arginine and Proline Metabolism	SSALY
			b3236	Citrate Cycle	MDH
			b1602+b1603	Oxidative Phosphorylation	THD2
			b0767	Pentose Phosphate Pathway	PGL
			b2975, b3603	Transport (Extracellular)	D-LACT2 , GLYCLT2r, L-LACT2
			b2492, b0904	Transport (Extracellular)	FORt

BioCAD results

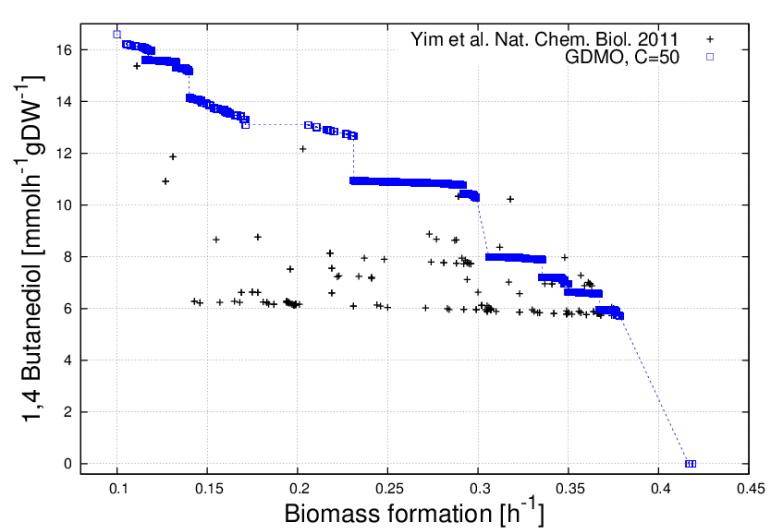
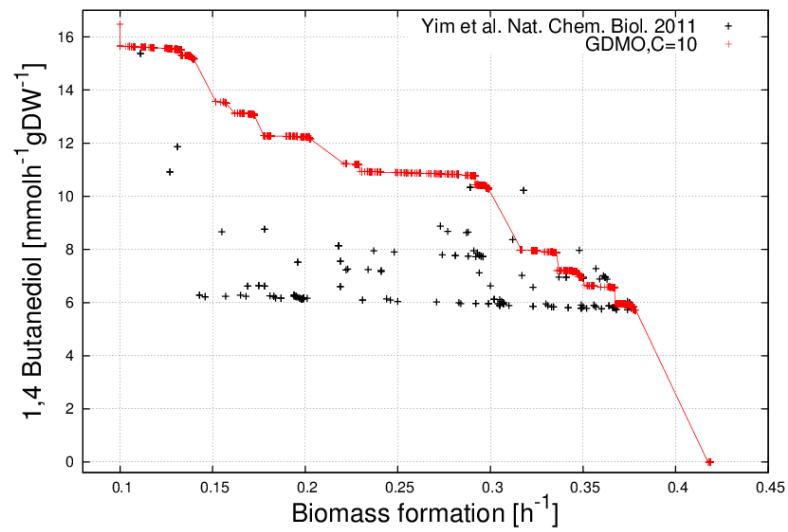
- **GDMO** considers the gene-protein-reaction (GPR) mapping and each bit of y is related to a gene set
- A gene set can be formed by
 - a single gene
 - more genes linked by a Boolean relationship
- The method in Yim et al. 2011 does not consider the GPR map, and turns off/on the flux of the reactions
- In order to compare our method with Yim et al. 2011 results, we also perform knockout research in the reaction space.

BioCAD results

Reaction space



Gene set space



Down- and Up- Regulation of Enzymes

Myristoyl-CoA Optimization for the iAF1260 E. coli: Fatty acids production

	BioCAD[**]	Redirector [*]
Biomass of the best strain	0.17 (+21.43%)	0.14
Myristoyl-CoA of the best strain	1.62 (+5.19%)	1.54
CPU time [s]	2400s	15200s

Anaerobic condition. Glucose uptake rate 8mmol-1 gDW-1.

Notable strain we obtain **dominates** the one obtained by G. Church et al [*].

[*] G. Rockwell, N. J. Guido and G. M. Church. *Redirector: designing cell factories by reconstructing the metabolic objective*. PLoS Computational Biology 9, 1, 2013.

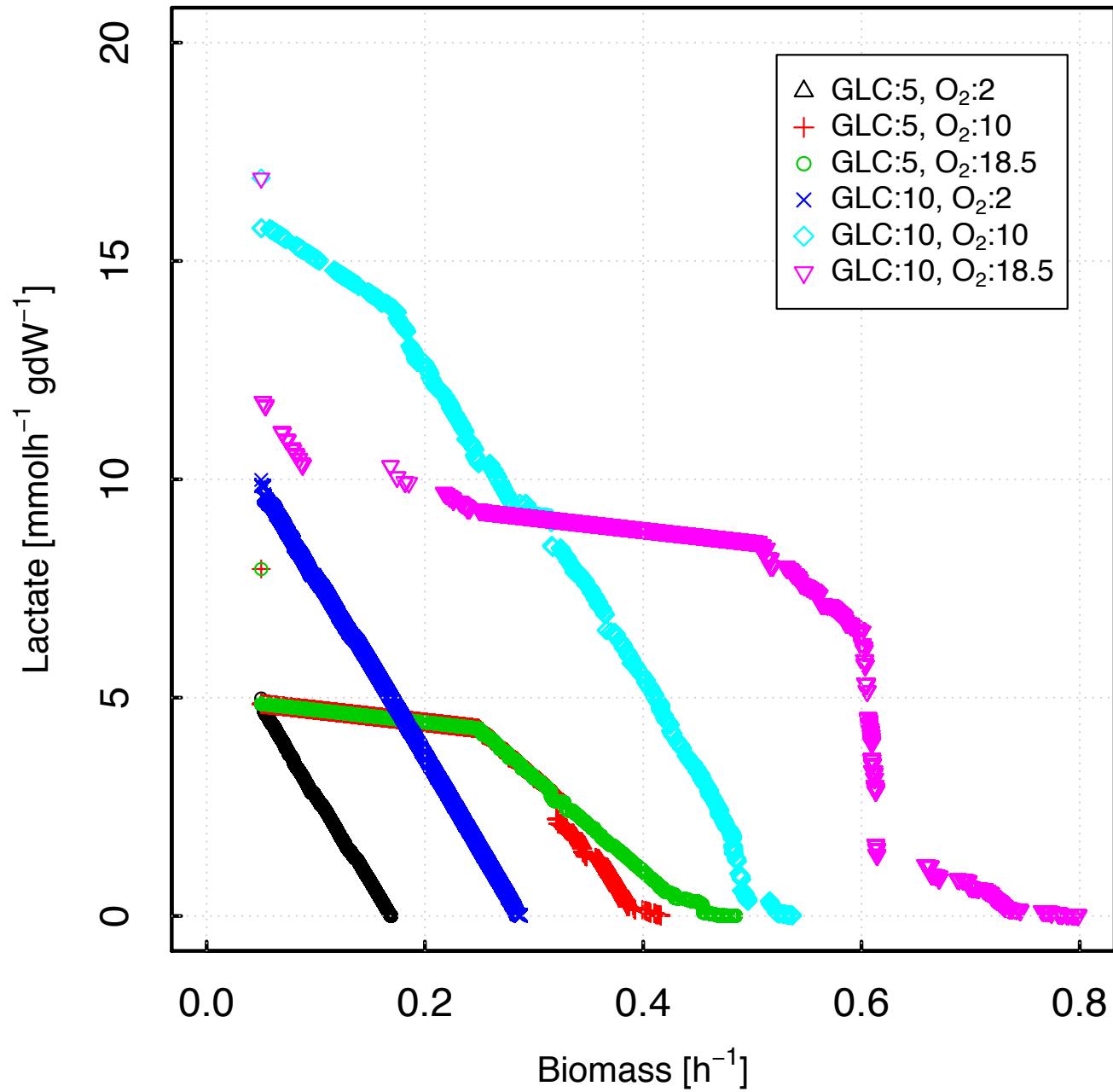
[**] Nicosia et al, IEEE Transactions on Biomedical Circuits & Systems, 2015.

Designing BioPlastic: Polylactic acid from Lactate acid production in *S. cerevisiae*

Lactate Production in *S. cerevisiae* by Redesigning the Metabolic Networks

- Organism: *Saccharomyces cerevisiae* S288c
- Model: iMM904
- Genome: PRJNA128
- Metabolites: 1226
- Reactions: 1577
- Genes: 905
- Database: <http://bigg.ucsd.edu/models/iMM904/>
- Publication PMID: 19321003
- Mo ML, Palsson BO, Herrgård MJ., Connecting extracellular metabolomic measurements to intracellular flux states in yeast. *BMC Syst Biol.* 2009 Mar 25;3:37. doi: 10.1186/1752-0509-3-37.

Lactate Production and Biomass Optimization in *S. cerevisiae*



A complete Computational Flow for Biological Design Automation

SA: SoSA, RoSA, PoSA

IA: Genotype-Phenotype relationships

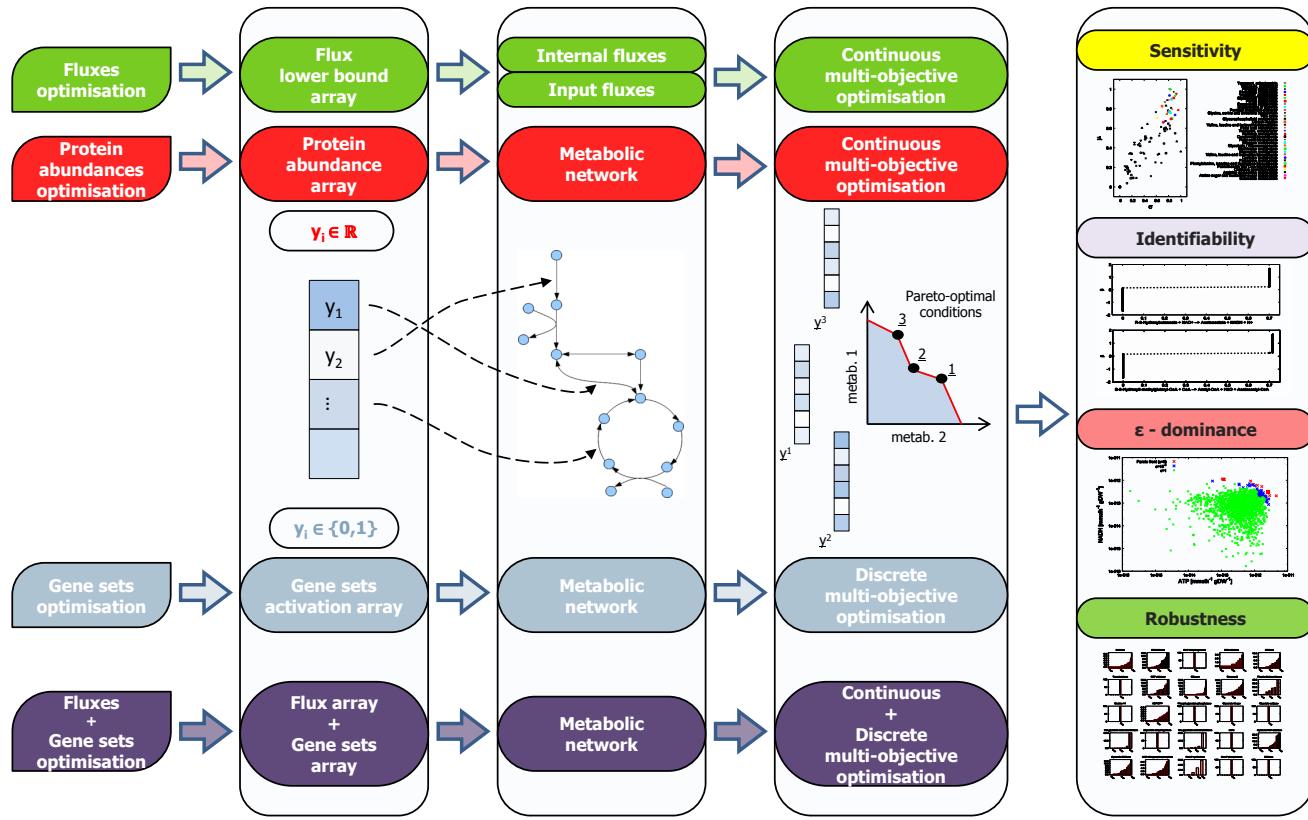
RA: LR, GR, GlocalR

Opt: SOO, MOO

Models: ODEs, DAEs, FBA, FBA-GPR.

Systems: Pathways, Organelles & Organisms

Conclusions



Results

1. 1,4 Butanediol Production in E. coli
2. ATP maximization in the Mitochondrion
3. Down- and Up- regulation of Enzymes for Fatty acids production
4. BioPlastic production by Engineered Yeast

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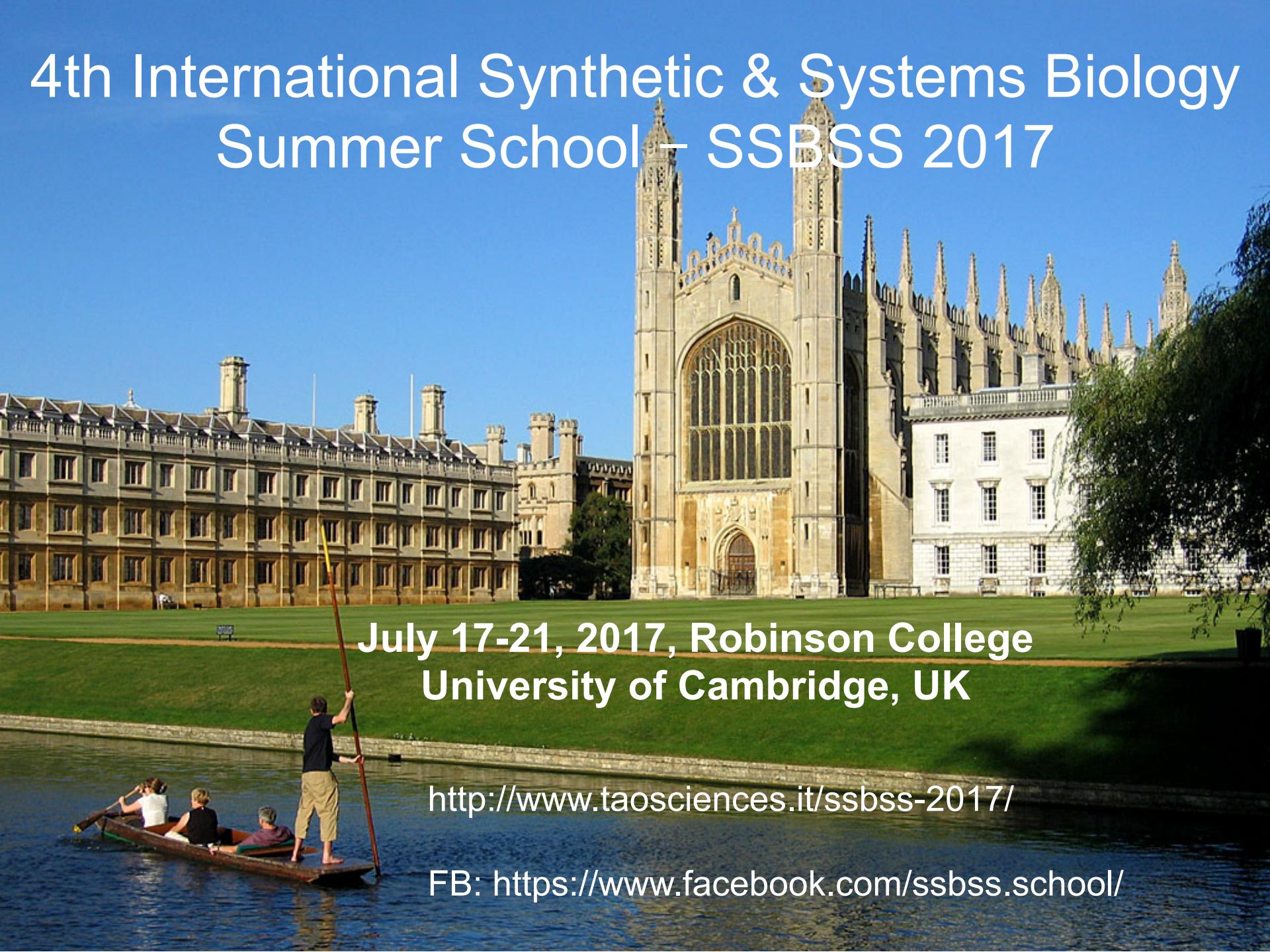
Piero Conca, CNR – Catania, Italy

Giorgio Jansen, University of Catania, Italy

Andrea Patanè, University of Catania, Italy

Andrea Santoro, University of Catania, Italy

4th International Synthetic & Systems Biology Summer School – SSBSS 2017

A scenic view of King's College Chapel in Cambridge, UK, with a punt on the River Cam in the foreground.

**July 17-21, 2017, Robinson College
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